# REMOVAL OF INDIGO CARMINE DYE FROM AQUEOUS SOLUTION USING LOW COST ADSORBENT: KINETIC AND THERMODYNAMIC STUDY

Pramod Jamdade<sup>1</sup>, Dr.Sanjay Ubale<sup>2</sup>

1. Assistant Professor, Department of Chemistry, SRM College, Kudal - 416520 (MS), India

2. Associate Professor, Department of Chemistry, Deogiri College, Aurangabad- 431001,

(MS), India.

**ABSTRACT:** The batch adsorption experiments were carried out to investigate the adsorptive removal of Indigo Carmine dye from aqueous solution using kokum (*Garcinia Indica*) leaf powder. The effect of various process parameters such as contact time, adsorbent dose, pH, initial concentration and temperature on removal of Indigo Carmine were studied. The equilibrium adsorption data were best represented by Langmuir and Freundlich isotherm models. From the experimental data, it was found that removal of Indigo Carmine by kokum leaf powder follows pseudo second order kinetics with regression coefficient value R<sup>2</sup>= 0.995. The value of R<sub>L</sub> and thermodynamic parameters such as  $\Delta G^0$ ,  $\Delta H^0$  and  $\Delta S^0$  indicated that removal of Indigo Carmine by Kokum leaf powder is spontaneous, endothermic and favorable. Thus kokum leaf powder is found to be effective adsorbent for the adsorptive removal of dyes from waste water.

Keywords: Indigo Carmine, Kokum leaf powder, Adsorption, Kinetics, Langmuir isotherm.

## I. INTRODUCTION

Azo dyes are the compounds that contain azo group (N=N) substituted aromatic molecules. Every year, there are more than  $10^4$  dyes produced worldwide (Nigam et.al..2000). These dyes are mostly used in textile, leather, cosmetic, paper, plastic and pharmaceutical industries (Gogate, P.R.; Pandit, A.B, 2004). They are synthetic, stable, non-biodegradable and carcinogenic in nature and have adverse effect on human beings (G., McKay 1982, McKay., S., J. et.al.1981). The discharge of these dyes into natural water sources without proper treatment causes environmental pollution and affect aquatic life (Kadirwelu.k. et.al 2003, Wang Y. et.al. 2004). Therefore their removal from waste water becomes matter of environmental concern. In the past, various dye removal methods have been used by different researchers like adsorption, coagulation, electro osmosis, ion exchange, membrane filtration etc. but in these methods, adsorption in the found to be effective and most widely used method. A large number of low cost adsorbents such as Almond tree bark, Azardichta indica leaf (Bhattacharya, Sharma), Teak tree bark (Satish Patil et.al. 2012) sunflower stalk (Sun G., Xu X 1997), rice husk (Singh D.K., Srivastava N. 2001) have been used for the removal of dyes from wastewater.

In present study, the adsorption of Indigo carmine by Kokum leaf powder (KLP) as the low cost adsorbent has been evaluated

## **II.MATERIALS AND METHODS**

## 2.1Preparation of kokum leaf powder as adsorbent (KLP)

Kokum plant leaves were dried in shadow, crushed and boiled in distilled water to remove colour and suspended dust.it was filtered and residue was treated with 20% formaldehyde and dilute sulphuric acid for 30 minutes. The residue was further washed with distilled water to remove free acid and dried at 100-120 °C for 8 hours, powdered and sieved to desired size and used for the study.

## 2.2Preparation of Indigo Carmine dye solution

The Indigo Carmine dyes solution of desired concentrations were prepared in distilled water using 1000 mg/L stock solution. The pH of solution was adjusted by using 0.1 N HCl or 0.1 N NaOH solutions

## 2.3Batch adsorption experiment

Batch adsorption experiments were carried by contacting 50 mL of 50 mg/L stock solution of indigo carmine and treated with 1.2g of KLP adsorbent. The effect of contact time, solution pH, adsorbent dose, initial dye concentration and temperature were evaluated. After desired time interval, sample solutions were filtered and residual dye concentration was determined using UV/VIS Spectrophotometer (Elico -1245) at 610 nm as  $\lambda_{max}$ . The equilibrium isotherm study was carried by mixing of 1.2 g adsorbent dose with various dye concentration of 10-50 mg/L for 60 minutes as equilibrium time at pH 6. The adsorption kinetics experiment was carried out using 1.2 g /L of adsorbent with dye concentration of 50 mg/L at pH 6 the dye solution was mixed at different time interval in the temperature range of 30 to 60 °C and residual dye concentration is determined by spectroscopic technique.

## **III.RESULTS AND DISCUSSION**

## 3.1 Effect of contact time

The adsorption experiment was carried out with 50 mg/L of Indigo carmine dye solutions was treated with 1.2 g of kokum leaf powder for 5 to 90 minutes at solution pH 6. The change in dye % removal with contact time has been shown in Figure 1 indicated that % dye removal was increased from 37.18 to 85.49 with increased contact time. The equilibrium was reached at 60 minutes .Similar observations were reported by other researchers (Khatri S.D., Singh M.K.2000).

## **3.2 Effect of dye solution pH**

The effect of solution pH on dye removal capacity of KLP was evaluated in the pH range of 2 to 10 with 50 ml dye solution for 50 mg/L concentration, 1.2 g adsorbent dose, 60 minutes contact time and 30 °C temperature. Figure 2 showed that 92.26 % of indigo carmine dye was removed at 2 pH and at pH 6, it was found to be 85.49 % and equilibrium was attained at pH 6. Similar results were reported by other workers (P. Bahadur et.al.1997)

# 3.3 Effect of dye initial concentration

The effect of initial dye concentration of indigo carmine (10 to 50 mg/L) on adsorption was studied with 50 mL volume, adsorbent dose 1.2 g /L, pH 6. From figure 3, it was observed that % removal of dye was decreased from 92.06 to 85.49 % whereas the amount of dye adsorbed increased with increase in concentration. It may be due to surface activity and monolayer formation in the given range of concentration. Similar results were reported by other researchers (Stephen J A, McKay G., and Kedar K. Y. 1989)

# 3.4 Effect of adsorbent dose

The effect of adsorbent dose was studied by the experiment carried out by taking 50 mL of 50 mg/L dye solutions and adsorbent dose was varied from 0.2 to 1.4 g. the removal of Indigo carmine was 36.23 to 85.49 % when treated with different doses of KLP as shown in Figure 4. The increase in dye removal % with increased dose is due to presence of more active sites on adsorbent surface (Namasivayam C., Yamuna R.T). The maximum removal of dye was found at 1.2 g dose

# **3.5 Effect of temperature**

To study the effect of temperature on removal of indigo carmine batch mode experiment was carried at the temperature ranging from 30 to 60 °C Figure 5, it was observed that, dye removal % increased from 86.02 to 90.57 % with increased temperature (Pandey K.K et.al.1988).





carmine by KLP



3.6

(1)

(2)

(3)

(4)



#### Adsorption isotherms

The adsorption isotherm indicates distribution of adsorbate adsorbent molecules at equilibrium state. The adsorption isotherm study was carried out with Langmuir and Freundlich isotherm models to evaluate best fit model. The linearized form of Freundlich isotherm can be given by (Singh A.K. 1988)

$$lnq_e = lnK_F + \frac{1}{n} lnC_e$$

Where  $q_e$  is the amount adsorbed (mg/g),  $C_e$  is dye equilibrium concentration (mg/L)  $K_F$  and n are freundlich constants of adsorption capacity and intensity respectively (Table 1) (Weber J.R.1972). The linear plot of ln  $q_e$  vs ln  $C_e$  given in Figure 6 The linear form of Langmuir isotherm to find out maximum monolayer adsorption capacity on adsorbent (I., Langmuir 1916)

$$C_e/q_e = 1/q_m b + 1/q_m C_e$$

Where  $C_e$  is equilibrium dye concentration (mg/L),  $C_e$  is dye equilibrium concentration (mg/L)  $q_e$  is the amount adsorbed (mg/g), b is adsorption equilibrium constant and  $q_m$  is maximum adsorption capacity of monolayer formation on surface. The values of qm and b are evaluated from slope, intercept and correlation coefficients (Table 1) from the plot of  $C_e/q_e$  vs  $C_e$  is given in Figure 7 the higher  $R^2$  indicate that adsorption of indigo carmine by KLP follows Langmuir isotherm model. The dimensionless separation factor  $R_L = 1/(1+bC_i)$  measure of adsorption occur (Hall K.R.1966). The  $R_L$  values between 0 to 1 indicative of the feasibility of adsorption process

#### 3.7 Adsorption kinetics

To determine the rate controlling mechanism of adsorption process such as mass transfer and chemical reactions pseudo first and pseudo second order kinetics models were used for experimental data. The linear Lagergren pseudo first order kinetic equation is given as (Ho. Y.S. and McKay, G. 2000)

$$logq_e - q_t = logq_e - (\frac{\kappa_1}{2,303})t$$

Where  $q_e$  and  $q_t$  the amount adsorbed (mg/g) at equilibrium and at time t,  $K_1$  is pseudo first order rate constant. The values of  $K_1$  and can be evaluated from slop and intercept of plot of  $\log(q_e - q_t)$  vs t given in Fig.8 and Table 2.

The pseudo second order kinetic equation is written as (Ho. Y.S. and McKay, G. (1999))  

$$\frac{t}{t} = \frac{1}{2} + (\frac{1}{2}) t$$

$$q_t = K_2 q_t^2$$
  $q_e^2$   
Where  $q_t$  is the amount of dye adsorbed at time t (mg/g) and  $q_e$  is equilibrium amount adsorbed (mg/g),  $K_2(g/mg.min.)$  is pseudo second order rate constant. The plot of  $\frac{t}{q_t}$  vs t given in Fig.9 The correlation coefficient and similarities between  $q_{e \text{ cal.}}$  and  $q_{e \text{ exp.}}$  showed that adsorption of indigo carmine by KLP follows pseudo second order rate kinetics.

#### 3.8 Thermodynamics studies

Thermodynamic parameters such as  $\Delta G^0$ ,  $\Delta H^0$  and  $\Delta S^0$  were evaluated by following equations (Hossain M.A, et.al. 2013)

$$K_{c} = \frac{C_{0} - C_{e}}{C_{e}}$$

$$\Delta G^{0} = -RT \ln K_{c}$$

$$\ln K_{c} = \Delta S^{0}/R - \Delta H^{0}/RT$$
(5)
(6)
(7)

 $\Delta G^0$  values were obtained from equation (4)  $\Delta H^0$  and  $\Delta S^0$  were obtained from slope and intercept of a plot of  $ln K_c$  versus 1/T Figure 10 represented in Table 3. The values of Gibbs free energy change, enthalpy change and entropy change, showed that adsorption of Indigo carmine on kokum leaf powder was spontaneous, endothermic and favorable with increased randomness during adsorption

# Table: 1 Langmuir and Freundlich parameters for adsorption of Indigo Carmine on KLP

I	angmuir constants	Freundlich constants			
$q_m (mg/g)$	b (L/mg)	$R^2$	$K_{f}$	n	$R^2$
133.33	0.0378	0.986	8.72	1.611	0.987

# Table: 2 Langmuir and Freundlich parameters for adsorption of Indigo Carmine on KLP

Pseudo first order model			Pseudo Second order model				
$\begin{array}{c} q_{e(exp.)} \\ mg \ g^{-1} \end{array}$	$K_1$ min <sup>-1</sup>	R <sup>2</sup>	$q_{e(cal.)} \ mg\ g^{-1}$	$K_2$ min. <sup>-1</sup>	$q_{e\ (cal.)}\ mg\ g^{-1}$	h mg/g.min	R <sup>2</sup>
2.042	0.0571	0.967	1.448	0.0486	1.781	0.154	0.995

# Table: 3 Thermodynamic parameters for adsorption of Indigo Carmine dye by KLP

K <sub>c</sub>			$R_L$	$-\Delta G^0$	$\Delta H^0$	$\Delta S^0$	
303 <sup>0</sup> K	313 <sup>0</sup> K	323 <sup>0</sup> K	333 <sup>0</sup> K		kJmol <sup>-1</sup>	kJmol <sup>-1</sup>	Jmol <sup>-1</sup>
6.153	6.800	7.772	8.979	0.346	5.287	10.476	49.530

# V. CONCLUSIONS

In this study, the equilibrium, kinetics and thermodynamics of adsorption of indigo carmine by Kokum leaf powder has been investigated. The isotherm equilibrium data were best fit with both Freundlich and Langmuir isotherm equation with  $R^2 = 0.986$  to 0.997. The monolayer adsorption capacity  $q_m$  was found to be 133.3 mg/g. The correlation coefficient  $R^2$  and similarities between  $q_e$  cal. and  $q_e \exp$ , showed that Lagergren pseudo second order model best describes the kinetics of adsorption of indigo carmine by KLP. The change in Gibbs free energy, enthalpy and entropy, indicated that adsorption of Indigo carmine on kokum leaf powder was spontaneous, endothermic and favorable with increased randomness during adsorption process. Therefore Kokum leaf powder adsorbent can be better substitute for the expensive activated carbon.

# VI. REFERENCES

- 1. Nigam P, Armour G, Banat I M, Singh D, Merchant R, Bioresour. Technol, 72, (2000) 219
- 2. Gogate, P.R.; Pandit, A.B. A review of imperative technologies for wastewater treatment I: Oxidation technologies at ambient conditions. *Adv. Environ. Res.* 2004, 8, 501–551.
- 3. G., McKay .J. Chem. Tech. Biotechnol.., (1982) 32,759
- 4. McKay., S.,J., Allen., I., F., Meconney., M., S., Ottrbun, J. Colloid Interface Sci. 1981, 80 (2), 323
- Kadirvelu, K., et al., Utilization of various agricultural wastes for activated carbon preparation and application for the removal of dyes and metal ions from aqueous solutions. *Bio-resource technology*, 2003. 87(1): p. 129-132
- 6. Wong, Y., et al., Adsorption of acid dyes on Chitosan equilibrium isotherm analysis. *Process Biochemistry*, 2004. 39(6): p. 695-704.
- 7. K.G.Bhattacharyya, A. Sharma, kinetics and thermodynamics of methylene blue adsorption on Neem (Azardichta indica). *Dye pigments*;65:51-59
- 8. Satish Patil, Sameer Renukadas, Naseema Patel, Int. J. Environ.Sci.vol.3 No 1, (2012)
- 9. Sun G., and Xu, X., (1997). Sunflower stalk as adsorbent for colour removal from textile wastewater, *Indian Eng. Chem. Res.* 36, 808-812
- 10. Singh D.K., Srivastava N. (2001). Basic dyes removal from wastewater by adsorption on rice husk carbon., *Indian Journal of Chemical Technology*, 8(2), 133-139
- 11. Khatri S.D., Singh M.K., Water Air & Soil Pollution ,120,(3-4),283-294(2000)
- 12. P. Bahadur, M. Desai, A. Dogra, S. Vora & R.N. Ram, Indian J. Chem. 1997, 36 A,938
- 13. Stephen J A, McKay G., Kedar K Y H, J. Chem. Tech. Bio. Tech., 45 (1989) 291
- 14. Namasivayam C., Yamuna R.T., Amer. Dyestuff Rep. Aug. 235-239
- 15. Pandey K.K, Prasad G., Singh V.N., Water Air & Soil Pollution, 27, 287-292 (1988)
- 16. Singh A.K., Singh D.P., Pandey K.K. and Singh V.N., 1988 Wollastonite as adsorbent for removal of Fe (II) from water. J. of Chem. Techol., 42, pp39
- 17. Weber J.R., Journal for Physicochemical process for water quality control (John Wiley & Sons, New York )1972
- 18. I., Langmuir(1916) .The constitution and fundamental properties of solids and liquids , J. Am. Chem. Soc., 38(11), 2221-2295
- 19. Hall K.R., Egaltone L.C., Acrivos A., Vermeulen T., (1966) Pore and solid diffusion kinetics in fixed bed adsorption under constant pattern condition. *Ind.Eng.Chem.Fundam.*, 5: 212-219
- 20. Ho. Y.S. and McKay, G. (2000) the kinetics of sorption of divalent metal ions onto sphagnum moss pear, *water Research* ;34(3): 735-742
- 21. Ho. Y.S. and McKay, G. (1999) Pseudo-second order model for sorption processes. Proc. Biochem; 34(5): 451-465
- 22. Hossain M.A.,and Hassan M.T.(2013)Kinetic and thermodynamic study of adsorption of crystal violet on used black tea leaves., *Orbital Elec. J. Chem.* 5(3):148-15