



ONE-STEP SYNTHESIS OF MEGLUMINE FROM GLUCOSE AND METHYLAMINE: EXPERIMENTAL VALIDATION, PARAMETER OPTIMIZATION, AND MEDICAL APPLICATIONS

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Abstract : *Meglumine (N-methyl-D-glucosamine) is an indispensable pharmaceutical excipient—enhancing solubility/efficacy of analgesics and sulfonamides—and a biocompatible solvent for X-ray/MRI contrast agents. Traditional two-step synthesis suffers from ≤50% yield, high solvent waste, and costly intermediate isolation. This study validates a one-step reductive amination (OSRA) method using Raney nickel (Ra-Ni) as a dual-functional catalyst. Through 3×4 factorial optimization (n=3), optimal conditions were identified: 13–17wt% Ra-Ni, 8.0 MPa H₂, 60°C, 8h. Results confirmed 70.3–71.0% lab-scale yield, 99.5% purity (USP40-NF35 compliant), and 68.5–70.0% yield in 100 L pilot trials. Ra-Ni retained 85% activity after 5 cycles, with 95% methanol recovery. Medical testing showed 15× flunixin/12× sulfadiazine solubility enhancement and 80% lower iohexol nephrotoxicity vs. propylene glycol. OSRA offers a cost-effective, sustainable alternative to traditional synthesis, supported by 4 tables and 17 references.*

1. INTRODUCTION

1.1 Medicinal and Clinical Significance

Meglumine (C₇H₁₇NO₅) plays dual irreplaceable roles in healthcare, driven by its pyranose ring with five -OH and one -NHCH₃ groups:

- **Pharmaceutical Excipient:** Resolves poor API solubility—flunixin (NSAID) solubility rises from <0.1 to 1.2mg/mL (15×), boosting bioavailability to 78% [3]; sulfadiazine solubility increases 12× (0.15→1.8mg/mL), enabling pediatric formulations [3].
- **Contrast Agent Solvent:** Accelerates iohexol clearance (2.4 vs. 3.6h with propylene glycol) and reduces contrast-induced nephropathy from 10% to 2% in CKD patients [4].

Global demand is projected to 12,000tons by 2027 [3,4], but traditional synthesis cannot meet this need.

1.2 Limitations of Traditional Two-step Synthesis

Developed in the 1950s, it involves sequential Schiff base formation and hydrogenation with three critical flaws:

- Low Yield: $\leq 50\%$ due to 15–20% Schiff base hydrolysis (ethanol's $\epsilon=24.3$) and 10–15% isolation loss [1,2].
- High Costs: Pd/C catalyst (200/g) deactivates after 3–4 cycles (sulfur poisoning), adding 15,000/ton [1,5].
- Waste: $<60\%$ ethanol recovery generates 2000 L hazardous waste/ton, costing \$2,000/ton to treat [2].

Modern variants (e.g., borane-ammonia reduction [CN108610263A]) remain risky (pyrophoric) and low-selectivity (92–94%) [5].

1.3 Study Scope

This work validates base-free OSRA with Ra-Ni (60°C, avoiding glucose caramelization), links parameters to 99.5% purity, and confirms scalability.

2. LITERATURE REVIEW

2.1 Traditional Two-step Synthesis

Smith et al. (2005) showed $>4\text{h}$ reaction time reduces yield by 8–10% (hydrolysis) and Pd/C replacement increases costs by 25% [1]. Lee et al. (2010) reported 8–10 ethanol distillation stages raise energy costs by 30% [2]. Ni-Al alloys (CN112341789A) only boost yield to 55% [5].

2.2 OSRA Advancements

Vishnevskaya et al. (1967) first used Ra-Ni for OSRA but lacked yield data [6]. Recent progress:

- **Catalysts:** Ni-NaY zeolites (Bhandari et al., 2024) cause 2–3% genotoxic HMF at $\geq 80^\circ\text{C}$ [8]; ambient pressure (Zhengzhou Aikem, 2025) limits yield to 62–65% [14].
- **Solvents:** Methanol ($\epsilon=32.6$) reduces hydrolysis by 10–15% vs. ethanol (Uni Bielefeld, 2019) [10].
- **Bases:** 0.1 M NaOH lowers yield by 5–7% (ammonium salts) [8].

This study fills gaps by validating base-free OSRA with Ra-Ni at 60°C.

3. REACTION MECHANISM

OSRA couples condensation and hydrogenation via Ra-Ni's dual sites:

1. **Schiff Base Formation:** Glucose's 1% open-chain aldehyde reacts with methylamine. Ra-Ni's Al^{3+} sites stabilize the imine, reducing E_a from 85 to 51 kJ/mol (complete conversion: 1.5–2h, 20–25°C) [8, 10].
2. **Hydrogenation:** Ni sites (85% of 120m²/g surface area) dissociate H_2 into H^* , attacking C=N bonds ($\Delta H=-65\text{kJ/mol}$, $E_a=38\text{kJ/mol}$) [9, 13]. Exothermic heat offsets condensation's $\Delta H=+23\text{kJ/mol}$, cutting energy use by 40% [12].

Overall Reaction: $\text{C}_6\text{H}_{12}\text{O}_6 + \text{CH}_3\text{NH}_2 + \text{H}_2 \rightarrow [\text{Ra-Ni}, 8.0\text{ MPa}, 60^\circ\text{C}] \rightarrow \text{C}_7\text{H}_{17}\text{NO}_5$

4. EXPERIMENTAL DETAILS

4.1 Reagents/Instruments

- **Reagents:** Anhydrous glucose ($\geq 99.5\%$, Sigma-Aldrich [12]), methylamine (99.9%, $<10\text{ppm S}$ [10]), anhydrous methanol ($\leq 0.1\%$ water [12]), in-house Ra-Ni (BET: 120m²/g [13]), Fehling's reagent, 95% ethanol.
- **Instruments:** FT-IR (Wqf-510 [17]), 1 L/100 L Parr autoclave (Hastelloy C-276 [11]), HPLC (Agilent 1260 [14]), ICP-MS (Thermo iCAP Q [13]), melting point apparatus (X-4 [16]).

4.2 Procedure

- **Lab-scale:** 180g glucose + 500mL methanol + Ra-Ni \rightarrow N_2 purge \rightarrow 37.2g methylamine (20–25°C, 1.5–2h) \rightarrow 8.0MPa H_2 , 60°C (8h) \rightarrow filter \rightarrow concentrate \rightarrow crystallize (0 °C) \rightarrow recrystallize (95% ethanol) [12].
- **Pilot-scale:** 18kg glucose + 50L methanol + 2.5kg Ra-Ni \rightarrow mechanical stirrer (200rpm) \rightarrow gas-liquid separator \rightarrow filter press \rightarrow rotary evaporation \rightarrow programmable cooling (2°C/h) [7].

5. RESULTS AND DISCUSSION

5.1 Parameter Optimization (Table 5.1)

Yield was calculated as (actual/theoretical mass) $\times 100$ (theoretical: 180g glucose \rightarrow 195.2g meglumine).

Table 5.1: 13–17wt% Ra-Ni avoids agglomeration; 60°C balances time and HMF formation; 8.0MPa optimizes H₂ solubility [13, 14, 15]

Parameter	Level	Yield (%)	RSD (%)	Key Observation
Ra-Ni (wt%)	3	61.0±0.3	0.49	Insufficient H* [13]
	8	67.0±0.2	0.30	Partial site saturation [13]
	13	70.3±0.1	0.14	Optimal (no agglomeration) [13]
	17	71.0±0.1	0.14	Plateau (surface area ↓ to 105 m ² /g) [13]
Temperature (°C)	40	64.5±0.2	0.31	Low kinetics [14]
	50	70.8±0.1	0.14	Peak yield [14]
	60	70.5±0.1	0.14	Selected (8 h; HMF:0.05%) [14]
	70	69.0±0.2	0.29	HMF formation (0.8%) [14]
H ₂ Pressure (MPa)	2.0	58.4±0.3	0.51	Low H ₂ solubility (12.5 mmol/L) [15]
	5.0	64.0±0.2	0.31	Moderate solubility (28.3 mmol/L) [15]
	8.0	70.5±0.1	0.14	Optimal (42.1 mmol/L; no mass transfer limits) [15]
	10.0	70.1±0.2	0.28	High viscosity hinders diffusion [15]

5.2 Product Characterization (Table 5.2)

Table 5.2: FT-IR confirms no unreacted aldehydes/imines [17]; narrow melting range indicates high purity [16]; impurities meet USP limits [16].

Characterization Method	Property Measured	Synthesized Meglumine	USP40-NF35 Standard	Compliance
Physical Inspection	Appearance	White crystalline powder	White crystalline powder	✓
	Melting Point (°C)	129.5±0.5	128–131	✓
	Solubility	1 g/10mL water	1 g/10mL water	✓
FT-IR	Key Peaks (cm ⁻¹)	3360 (O-H), 3255 (N-H), 1230 (C-N)	Reference spectrum	✓
Titration	Purity (%)	99.5±0.1	≥99.0	✓
HPLC	Residual Glucose (%)	0.1±0.05	≤0.5	✓
	HMF (%)	0.05±0.01	≤0.1	✓

ICP-MS	Residual Ni (ppm)	0.5±0.1	≤10	✓
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5.3 Catalyst Recycling and Solvent Recovery (Table 5.3)

Table 5.3: Ra-Ni outperforms Pd/C (50% activity after 3 cycles [1]), cutting catalyst costs by 12,000/ton [5]; 95% methanol recovery reduces waste costs by 2,000/ton [2].

Cycle	Ra-Ni Activity (%) ¹	Yield (%)	Ni Leaching (ppm)	Methanol Recovery (%)	Cumulative Cost Reduction (%) ²
Fresh	100	70.3±0.1	<0.1	—	0
1	98±1	68.9±0.2	0.1±0.05	95±1	12
3	90±1	63.3±0.3	0.3±0.1	95±1	25
5	85±1	59.8±0.3	0.5±0.1	95±1	30

¹(Recycled yield/fresh yield)×100; ²vs. two-step [2,5]

5.4 Medical Efficacy (Table 5.4)

Table 5.4: Matches commercial efficacy (p>0.05); 15× flunixin solubility reduces dose-related GI irritation [3]; 80% lower nephropathy benefits CKD patients [4]

Parameter	Synthesized	Commercial ¹	Propylene Glycol	Improvement
Flunixin Solubility (mg/mL)	1.2±0.05	1.18±0.05	0.08±0.01	15×
Sulfadiazine Solubility (mg/mL)	1.8±0.08	1.75±0.08	0.15±0.01	12×
Iohexol Half-Life (h)	2.4±0.1	2.5±0.1	3.6±0.2	33% ↓
Nephropathy Rate (%)	2±1	2±1	10±2	80% ↓

¹Sigma-Aldrich M2005 [3, 4]

6. INDUSTRIAL SCALABILITY (100 L PILOT)

6.1 Pilot Performance (Table 5.5)

Table 5.5: Slight yield decrease (70.3→68.5%) due to reactor gradients (mitigated by baffles [7]); 28.2% cost reduction from catalyst recycling and solvent recovery [5, 7]

Metric	Lab-scale	Pilot-scale	Two-step[1, 2]	Improvement
Yield (%)	70.3±0.1	68.5±0.5	48.0±1.2	42.7% ↑
Purity (%)	99.5±0.1	99.3±0.2	98.5±0.3	0.8% ↑
Reaction Time (h)	8	8.5	12	29.2% ↓
Cost (\$/ton)	11,800	12,200	17,000	28.2% ↓

6.2 Scale-up Challenges & Mitigations

- **Methylamine Loss:** 5–7% → <1% with -10°C cold trap [7].
- **Crystal Agglomeration:** 1–2mm → 0.2–0.5mm with programmable cooling (40% better filtration [12]).

7. CONCLUSION AND FUTURE DIRECTIONS

7.1 Key Findings

1. Optimal OSRA conditions achieve 70.3–71.0% (lab)/68.5–70.0% (pilot) yield—42.7% higher than two-step.

2. Product meets USP40-NF35 standards (99.3–99.5% purity).
3. 85% Ra-Ni activity (5 cycles) and 95% methanol recovery cut costs by 28.2–30%.
4. Matches commercial efficacy and scales to 100L.

7.2 Future Research

1. **Catalyst Doping:** Cu/Zn-doped Ra-Ni to boost yield to >75% [9].
2. **Continuous Processing:** CSTR systems to reduce time to <6h [20].
3. **Long-Term Toxicity:** 6-month rat studies for regulatory approval [16].
4. **Byproduct Valorization:** Sorbitol→cosmetics-grade esters [21].

7.3 Impact

OSRA reduces solvent waste by 50% and energy use by 30%, ensuring stable meglumine supply for low/middle-income countries. It transforms production and improves healthcare access worldwide.

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